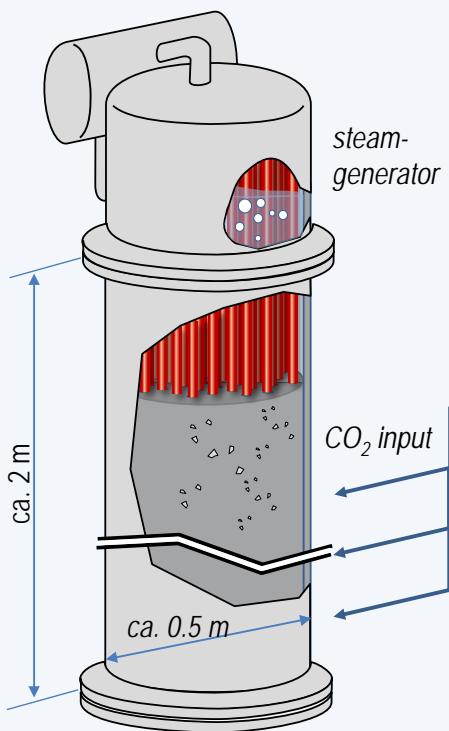


7<sup>th</sup> Intl. Conf. on Engineering for Waste and Biomass Valorisation,  
02.07.2018

# Peak-Load High-Temperature Carbonate Storage



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Motivation

Concept

Charge

Discharge

Summary

## 1. Motivation

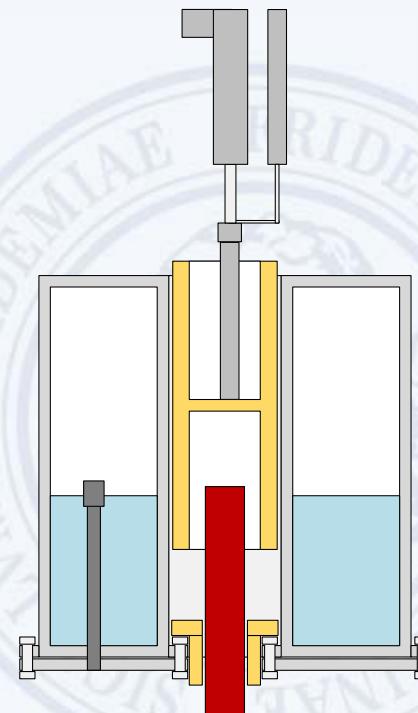
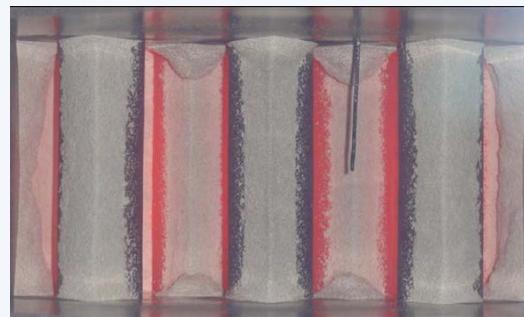
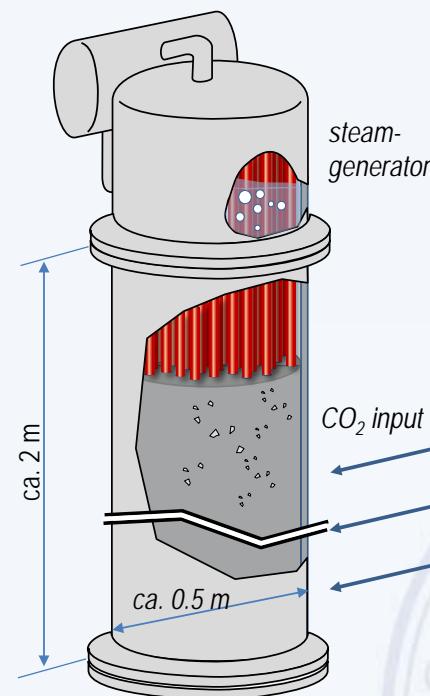
## 2. Concept

## 3. Charging Concept

## 4. Discharge

- a) Fluidized Bed
- b) Steam Generator

## 5. Summary



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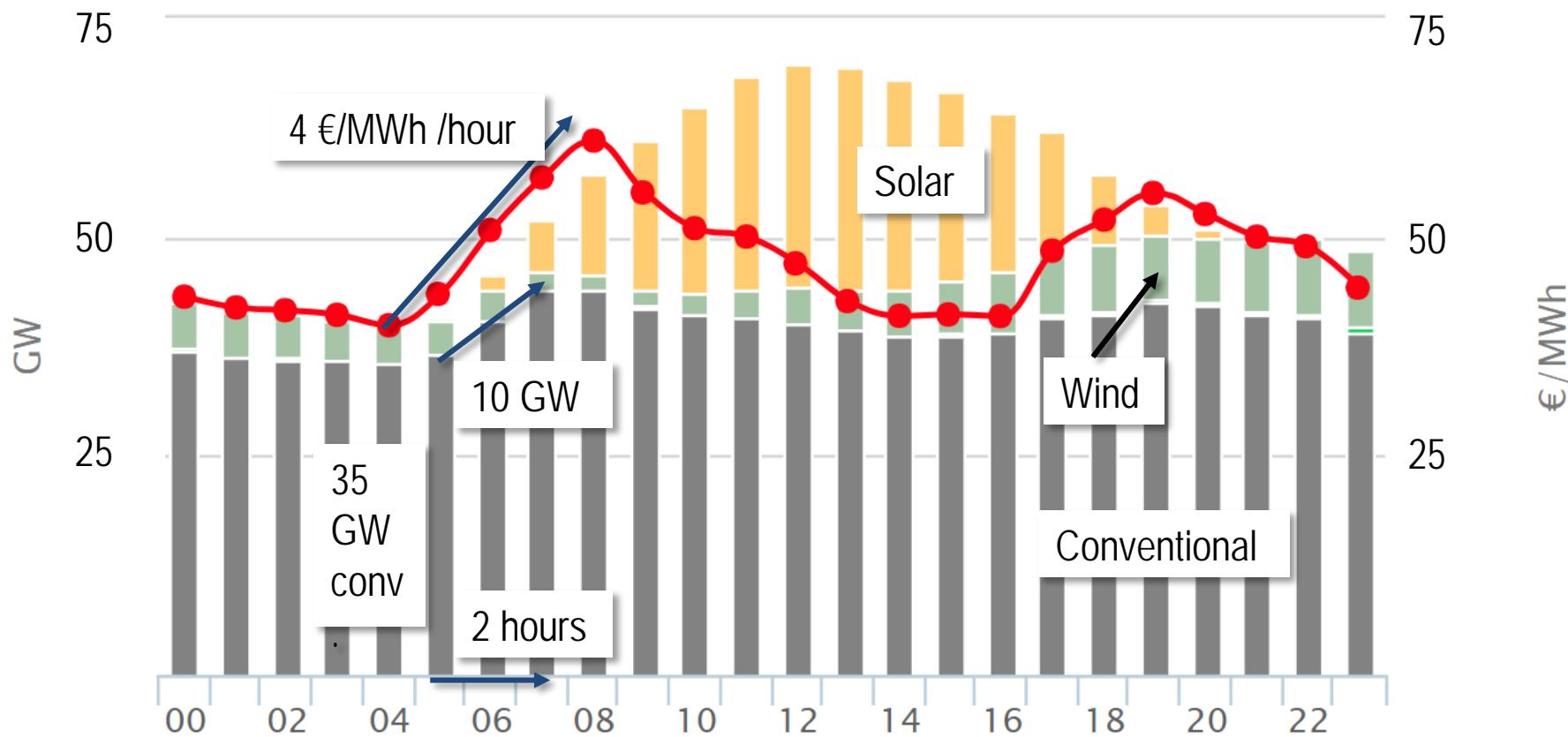


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27.06.2018

Deutschland

# Electricity Generation and Prices at Energy Exchange Market in Germany



<https://www.eex-transparency.com>

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# Why Peak-Load High-Temperature Storage?

Motivation

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Summary

## power demand peaks

- high **load gradients** in morning and evening hours
- additional load fluctuation through renewables (> 35 % in Germany 2017)
- conventional power plants not flexible enough to compensate
- → need to enhance ability of steam power plants for load flexibility

## high temperature storage → solution

- load shift: dynamic (high power density) and flexible (quick start up)
- high storage capacity (cheap material)
- but: short operating times:
  - high electricity prices available to make it feasible
  - lower investment costs through integration with existing infrastructure

# Why Peak-Load High-Temperature Storage?

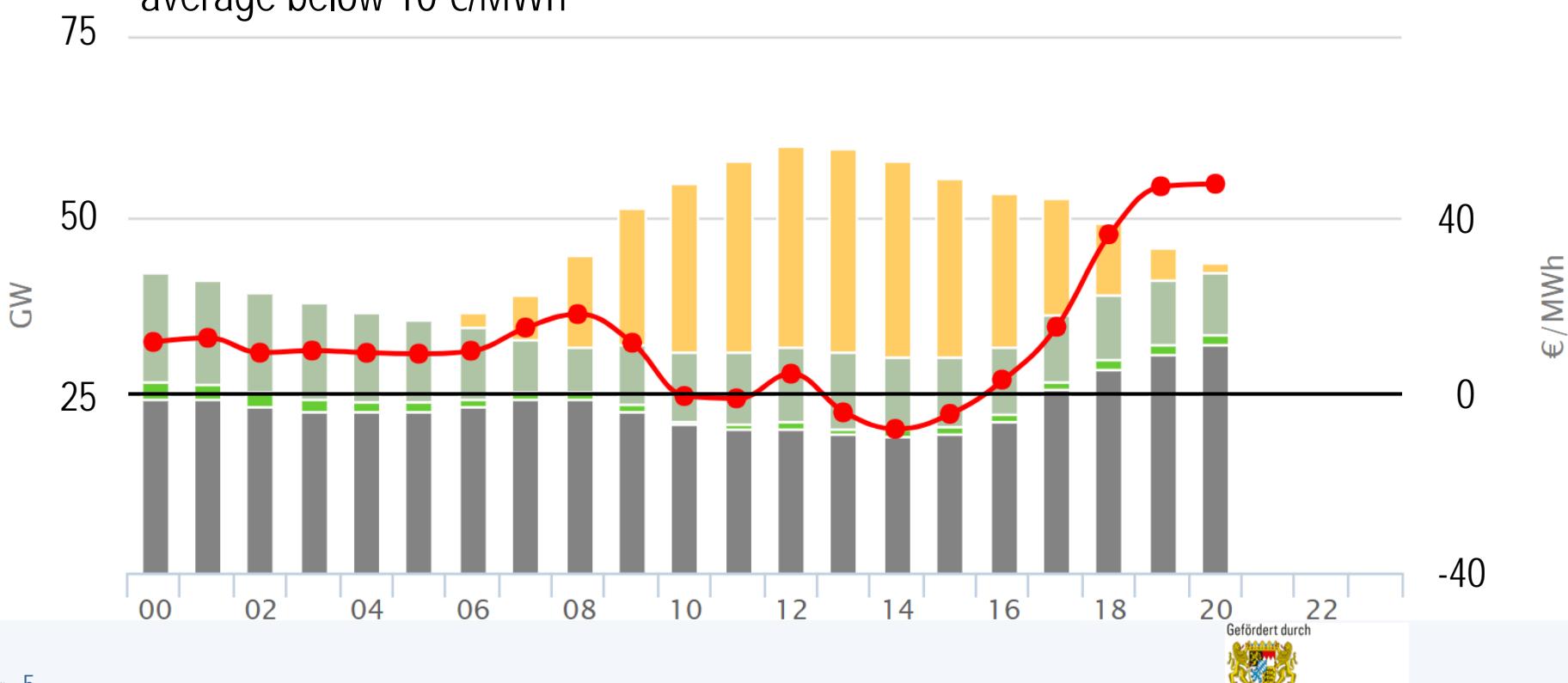
Motivation

01.07.2018

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## Electricity Generation:

- negative prices (min: -7.7 €/MWh)
- average below 10 €/MWh



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# Concept: High Temperature Carbonate Storage

Motivation

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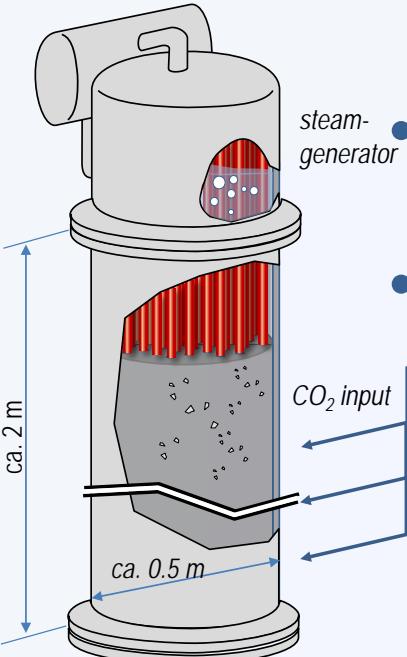
Summary

- calcination heated through **surplus electricity**
- carbonation for discharge/heat output to steam generator



$$\Delta h_R^0 = 182 \text{ kJ/mol}$$

→ high energy/power density (630 kWh/m<sup>3</sup>//65 kW/m<sup>3</sup> reactor volume)



- sodium heat pipes: ideal heat transfer and isothermal temperature profile
  - increased reaction zone, high power output possible
- Pressure variation for fast change variation of equilibrium at 850 °C
  - → no need for heating up or cooling down
  - even if storage cools down a little, carbonation works even better

# Function of heat pipe

Motivation

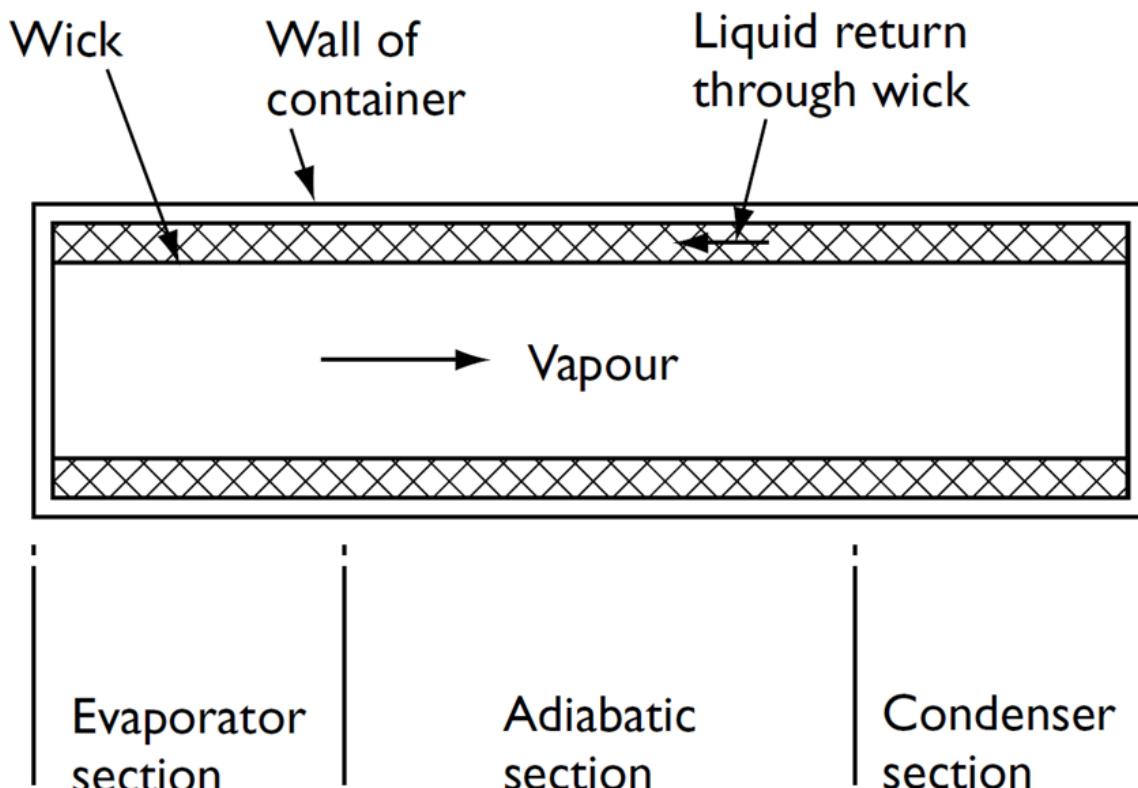
Concept

Charge

Discharge

Summary

- isothermal temperature over whole length
- evaporation/condensation heat transfer >> latent/convection heat transfer



Quelle: Kew, D. R. (2007). Heat Pipes Theory, Design and Applications; 5th Edition

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und Technologie

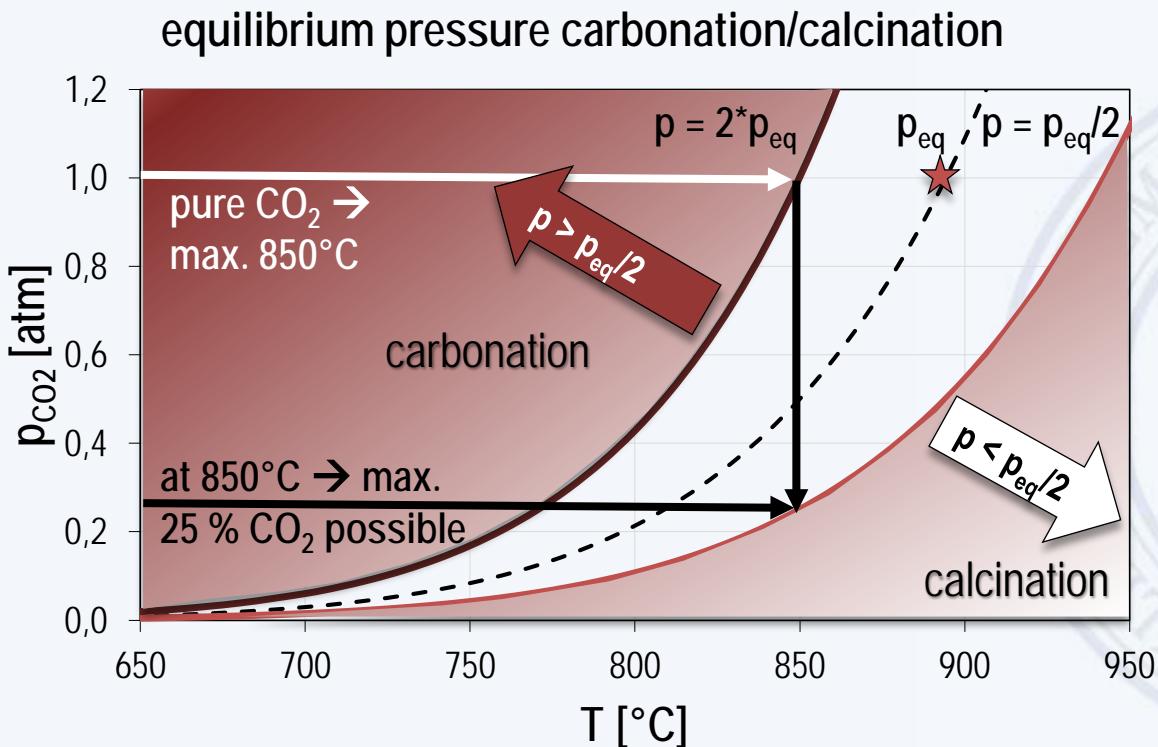
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# Equilibrium

Motivation  
Concept  
Charge  
Discharge  
Summary

- carbonation with high  $p_{CO_2}$  and „low“ temperatures
- calcination with low  $p_{CO_2} (< \frac{1}{2} p_{eq})^1$  and „high“ temperatures
- TGA result: at 850 °C similar reaction times carbonation/calcination in TGA

} isothermal?!



<sup>1</sup> Kubato et al. 2000 – Study of decarbonation of CaCO<sub>3</sub> for high temperature thermal energy storage

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# Project goals

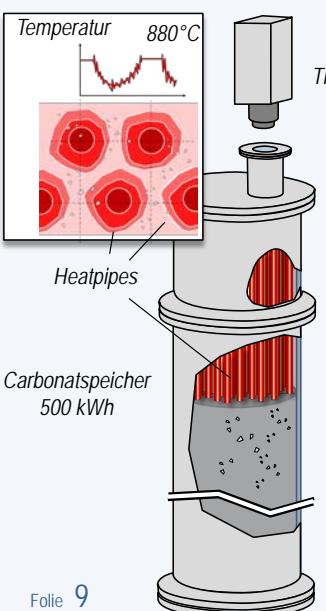
Motivation

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Summary



- proof-of-concept in pilot plant: 250 kWh, 20 kW<sub>th</sub>
  - isothermal temperature profile in carbonate bed through heat pipes
  - isothermal operation: carbonation and calcination at same temperature level
- experimental investigations:
  - fluidisation with varying CO<sub>2</sub> partial pressure
  - heat transfer measurements in fixed/fluidised bed
  - optimisation of process conditions
    - dynamic power output
    - cyclic stability and cycle number of CaO/CaCO<sub>3</sub>
- feasibility analysis:
  - technical and economical investigation
  - steam injection to different pressure levels in power plants

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# Charging/Heating

Motivation

Concept

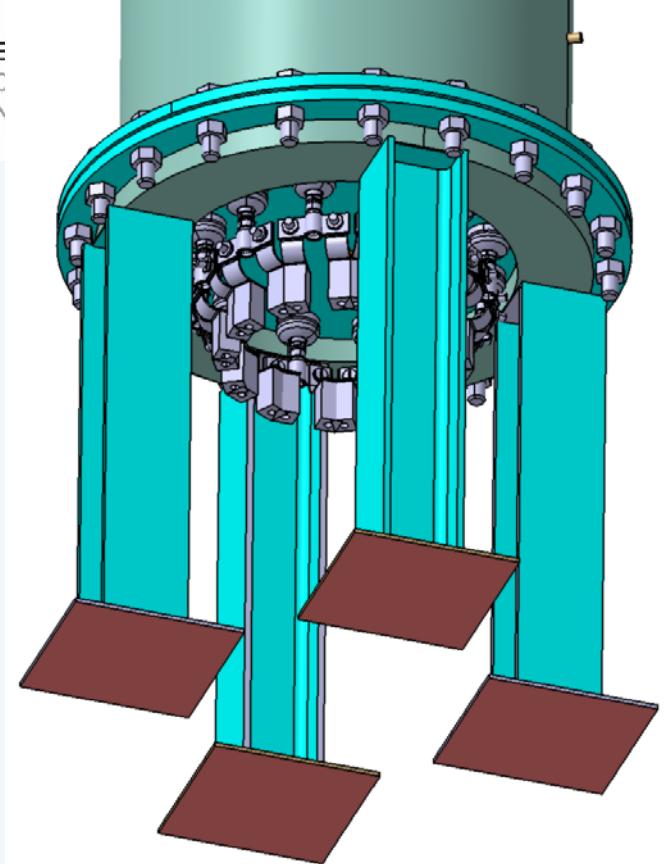
Charge

Discharge

Summary

## design challenges

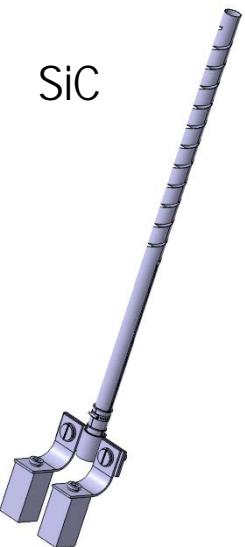
- 20 kW electrical heating
- 2 kW/heat pipe at 1000 °C
- heat transfer in & out with heat pipes
- minimisation of losses during storage



## idea

- integration of heating elements in heat pipe bottom

	heating wire Kanthal	SiC heating element
surface load density	up to 2 W/cm <sup>2</sup>	up to 16.5 W/cm <sup>2</sup>
stability up to	1300 °C	1600 °C
required heated length	2 m	0,25 m



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# Charging/Heating

Motivation

Concept

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Summary

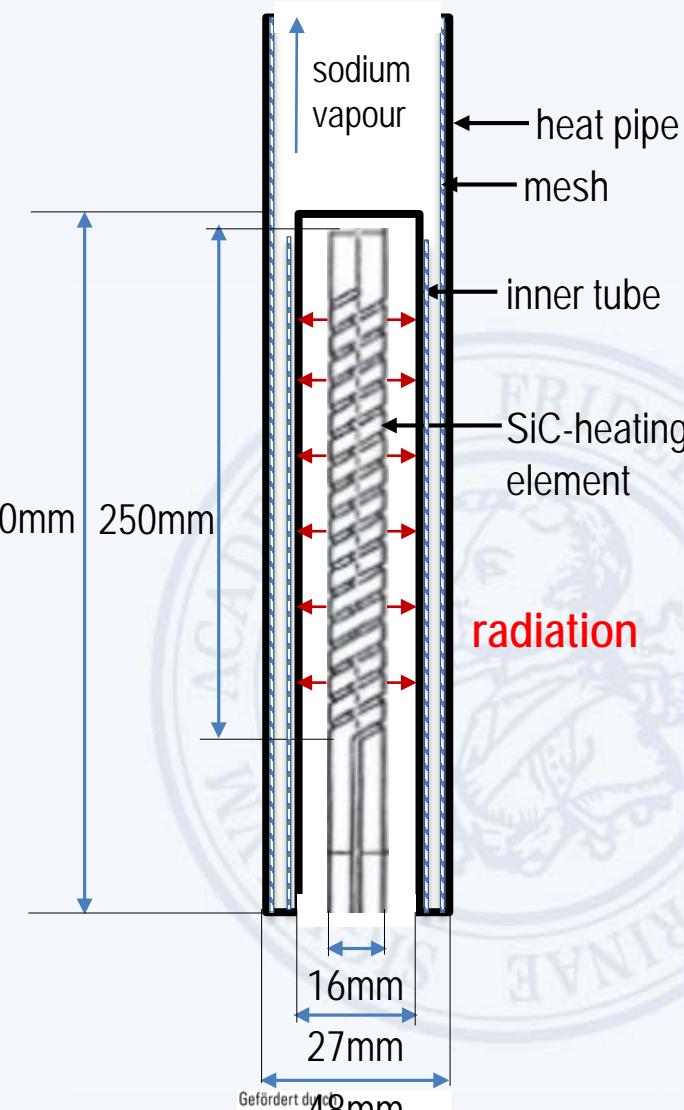
## challenges

- electrical insulation, fragility, thermal expansion
- temperature control essential
- HP dry-out: inner mesh & sodium filling ratio

Location	Temperature
CaCO <sub>3</sub>	ca. 850°C
heat pipe	ca. 900°C
inner tube	ca. 930°C
SiC-element	ca. 1250°C

$$\Delta T \approx 50K$$

$$\Delta T \approx 300K$$



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## first results

- 2 kW transferred
- increased heat transfer resistance in heating zone through new HP concept → solve!



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# Discharge with fluidized bed carbonation

Motivation

Concept

Charge

Discharge

Summary

## challenge

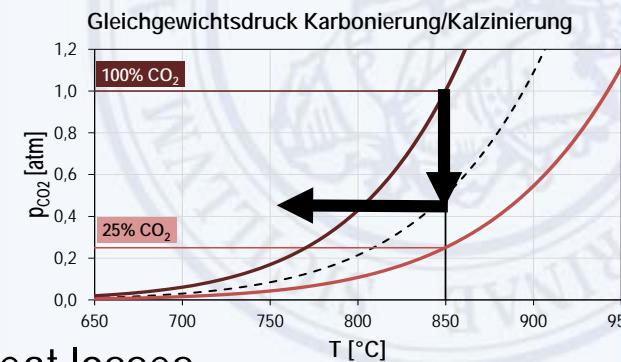
- CO<sub>2</sub> flow/fluidisation diminishes in reactor
- limitation for heat transfer: heat transfer from CaCO<sub>3</sub> to heat pipes

→ sufficient/stable fluidization in whole reactor necessary ( $u/u_0 > 1.5$ )!

## options

1. reactor diameter < 0.4 m. but: constant capacity makes it taller
2. higher CO<sub>2</sub> volume flow. but: added heat losses/higher power output
3. fine particles < 200 µm for lower  $u_{mf}$ , but: cohesive
4. dilution with N<sub>2</sub>/steam during carbonation
  - higher fluidisation at bed surface
  - possibly higher cyclic CaO conversion
  - but: decreasing operating temperature, added heat losses

→ compromise to be found in pre-tests



# Discharge/Steam Generator

Motivation

Concept

Charge

Discharge

Summary

## challenge

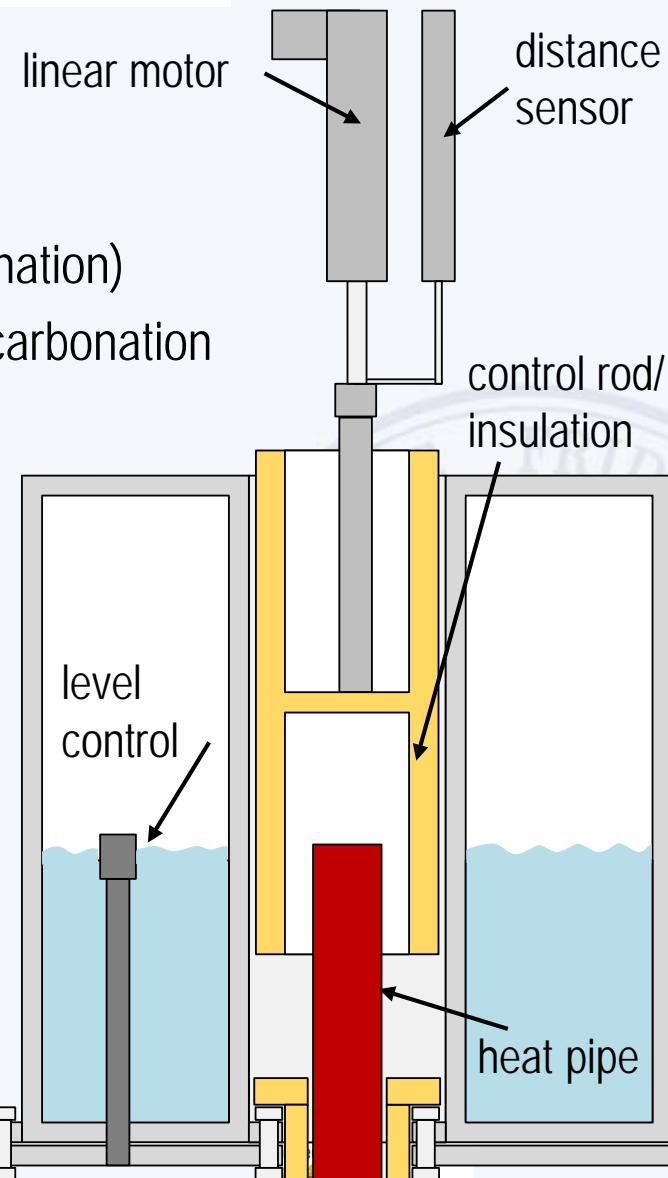
- insulation during storage and charging (calcination)
- dynamic & flexible power generation during carbonation
- → dynamic control and safety

## experimental

- 1 HP, pressure up to 5 bar, saturated vapour
- characterisation of operating behaviour depending on power demand
- fluidised bed reactor under construction

## results

- first tests with 20 mm microporous insulation
- 350 W loss over steam generator for 850°C heat pipe



# Summary

*Thank you for your Attention!*

Motivation  
Concept  
Charge  
Discharge  
Summary

- **isothermal** high temperature carbonate storage can support conventional power plants during **high load gradients**
- multiple applications for integration to power plant
- variation of  $p_{CO_2}$  allows quick switch between charge/discharge mode and variety of temperature levels
- currently test of different components regarding charge/discharge
  - compromise for fluidised bed operation
- construction of pilot plant in 2019 for proof-of-concept
- **optimisation of operating conditions**
  - for dynamic operation
  - for cyclic stability of  $CaO/CaCO_3$

